Master
in Space Science and Technology

Thermal engineering

Isidoro Martínez

POLITÉCNICA

Thermal engineering

- **Thermodynamics**
  - Basics
    - Energy and entropy
    - Temperature and thermometry
    - Variables: state properties, process functions
    - Equations of state, simple processes
    - Phase change
  - Applied:
    - Mixtures. Humid air (air conditioning)
    - Thermochemistry (combustion)
    - Heat engines (power generation)
    - Refrigeration (cold generation)
    - Thermal effects on materials and processes
    - Thermofluiddynamic flow 1D…

- **Heat transfer (conduction, convection, radiation, heat exchangers)**

Thermodynamics

- **Basic thermodynamics**
  - The science of heat and temperature. Work. Energy. Thermal energy.
  - Energy and entropy. The isolated system. The traditional Principles
  - Generalisation (mass, momentum, energy): the science of assets (conservatives do not disappear) and spreads (conservatives tend to disperse)
  - Type of thermodynamic systems (system, frontier, and surroundings)
    - Isolated system: $\Delta m=0$, $\Delta E=0$
    - Closed system : $\Delta m=0$, $\Delta E\neq 0$
    - Open system : $\Delta m\neq 0$, $\Delta E\neq 0$
  - Type of thermodynamic variables
    - Intensive or extensive variables
    - State or process variables
  - Type of thermodynamic equations
    - Balance equations (conservation laws); e.g. $\Delta E_{\text{close-sys}}=W+Q$
    - Equations of state (constitutive laws); e.g. $pV=mRT$
    - Equilibrium laws: $S(U,V,n_i)_{\text{iso-sys}}(t)\to S_{\max}$ e.g. $\mathrm{d}S/\mathrm{d}U|_{V,n_i}=$uniform…
    - (Kinetics is beyond classical thermodynamics; e.g. $\dot{\vec{q}}=-k\nabla T$)
- **Applied thermodynamics**

Thermodynamics (cont.)

- **Basic thermodynamics**
- **Applied thermodynamics**
  - Energy and exergy analysis (minimum expense and maximum benefit)
  - Non-reactive mixtures (properties of real mixtures, ideal mixture model…)
  - Hygrometry (humid air applications: drying, humidification, air conditioning…)
  - Phase transition in mixtures (liquid-vapour equilibrium, solutions…)
  - Reactive mixtures. Thermochemistry. Combustion
  - Heat engines
    - Gas cycles for reciprocating and rotodynamic engines
    - Vapour cycles (steam and organic fluid power plants)
  - Refrigeration, and heat pumps
    - Cryogenics (cryocoolers, cryostats, cryopreservation…)
  - Thermal analysis of materials (fixed points, calorimetry, dilatometry…)
  - Non-equilibrium thermodynamics (thermoelectricity, dissipative structures…)
  - Environmental thermodynamics (ocean and atmospheric processes…)

Balance equations

Magnitude	Accumul		Production	Impermeable flux	Permeable flux
mass	$\mathrm{d}m$	=	0	$+0$	$+\Sigma \mathrm{d}m_e$
momentum	$\mathrm{d}(m\vec{v})$	=	$m\vec{g}\,\mathrm{d}t$	$+\vec{F}_A\,\mathrm{d}t$	$+\Sigma\vec{v}_e\,\mathrm{d}m_e - \Sigma p_e A_e \vec{n}_e\,\mathrm{d}t$
energy	$\mathrm{d}(me)$	=	0	$+\mathrm{d}W+\mathrm{d}Q$	$+\Sigma h_{te}\mathrm{d}m_e$
entropy	$\mathrm{d}(ms)$	=	dS_{gen}	$+\mathrm{d}Q/T$	$+\Sigma s_e \mathrm{d}m_e$
exergy	$\mathrm{d}(m\phi)$	=	$-T_0\mathrm{dS}_{gen}$	$+\mathrm{d}W_u+(1-T_0/T)\mathrm{d}Q$	$+\Sigma\psi_e \mathrm{d}m_e$

with $e=u+e_m=u+gz+v^2/2$

$$\mathrm{d}W=\int_{IF}F\mathrm{d}x=\int_{IF}M\mathrm{d}\theta,\quad W_u=W+p_0\Delta V$$

$$h=u+pv,\quad h_t=h+e_m$$

$$\mathrm{d}s=(\mathrm{d}u+p\mathrm{d}v)/T=(\mathrm{d}q+\mathrm{d}e_{mdf})/T,\ \ \mathrm{d}e_{mdf}\geq 0,\ \mathrm{d}S_{gen}\geq 0$$

$$\phi=e+p_0v-T_0s,\quad \psi=h_t-T_0s$$

Substance data

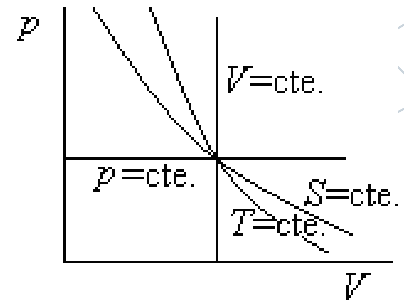
- **Perfect gas model**
  - Ideal gas: $pV=mRT$ or $pV=nR_uT$ ($R=R_u/M$, R_u=8.3 J/(mol·K))
  - Energetically linear in temperature: $\Delta U=mc_v\Delta T$
  - _Air data_: R=287 J/(kg·K) and $c_p=c_v+R$=1000 J/(kg·K), or M=0.029 kg/mol and $\gamma=c_p/c_v$=1.4
- **Perfect solid or liquid model**
  - Incompressible, undilatable substance: V=constant (but beware of dilatations!)
  - Energetically linear in temperature: $\Delta U=mc\Delta T$
  - _Water data_: ρ=1000 kg/m^3, c=4200 J(kg·K)
- **Perfect mixture (homogeneous)**
  - Ideal mixture $v=\sum x_i v_i^*,\quad u=\sum x_i u_i^*,\quad s=\sum x_i s_i^* - R\sum x_i \ln x_i$
  - Energetically linear in temperature: $\Delta U=mc_v\Delta T$
- **Heterogeneous systems**
  - Phase equilibria of pure substances (Clapeyron's equation) $\left.\frac{dp}{dT}\right|_{sat}=\frac{\Delta h}{T\Delta v}$
  - Ideal liquid-vapour mixtures (Raoult's law): $\frac{x_{V1}}{x_{L1}}=\frac{p_1^*(T)}{p}$
  - Ideal liquid-gas solutions (Henry's law): $\frac{c_{L,s}}{c_{G,s}}=K_{s,cc}^{dis}(T)$
- **Real gases. The corresponding state model, and other equations of state.**

Thermodynamic processes

- **Adiabatic non-dissipative process of a perfect gas:**

$$dE = dQ + dW \quad\rightarrow\quad dU = -pdV \quad\rightarrow\quad mc_v dT = -\frac{mRT}{V}dV$$

$$\rightarrow\quad \frac{dT}{T} + \frac{R}{c_v}\frac{dV}{V} = 0 \quad\rightarrow\quad Tv^{\gamma-1} = \text{cte.},\ pv^{\gamma} = \text{cte.},\ T/p^{\frac{\gamma-1}{\gamma}} = \text{cte.}$$



- **Fluid heating or cooling**
  - At constant volume: $Q=\Delta U$
  - At constant pressure: $Q=\Delta H=\Delta(U+pV)$
- **Adiabatic gas compression or expansion**
  - Close system: $w=\Delta u=c_v(T_2-T_1)$
  - Open system: $w=\Delta h=c_p(T_2-T_1)$

$$\eta_C \equiv \frac{w_s}{w} = \frac{h_{2ts}-h_{1t}}{h_{2t}-h_{1t}} \overset{\text{PGM}}{=} \frac{\left(p_{2t}/p_{1t}\right)^{\frac{\gamma-1}{\gamma}}-1}{T_{2t}/T_{1t}-1} \qquad \eta_T \equiv \frac{w}{w_s} \overset{\text{PGM}}{=} \frac{1-T_{1t}/T_{2t}}{1-\left(p_{1t}/p_{2t}\right)^{\frac{\gamma-1}{\gamma}}}$$

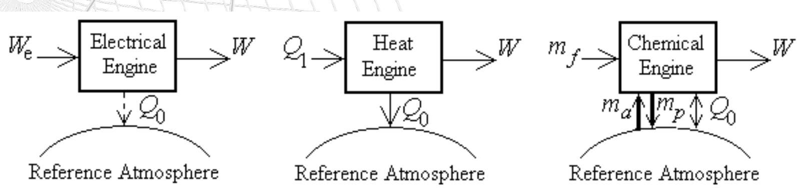
- **Internal energy equation (heating and cooling processes)**

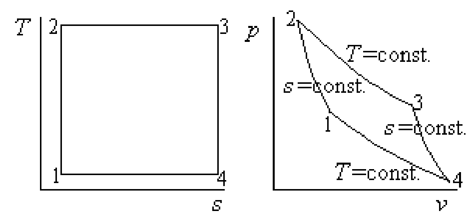
$$\Delta U \equiv \Delta E - \Delta E_m = Q + E_{mdf} - \int pdV$$

- **One-dimensional flow at steady state**

$$\dot{m}_{\text{in}} = \dot{m}_{\text{out}} = \rho v A = \rho\dot{V} \qquad \Delta h = w + q \qquad w = \int\frac{dp}{\rho} + \Delta e_m + e_{mdf}$$

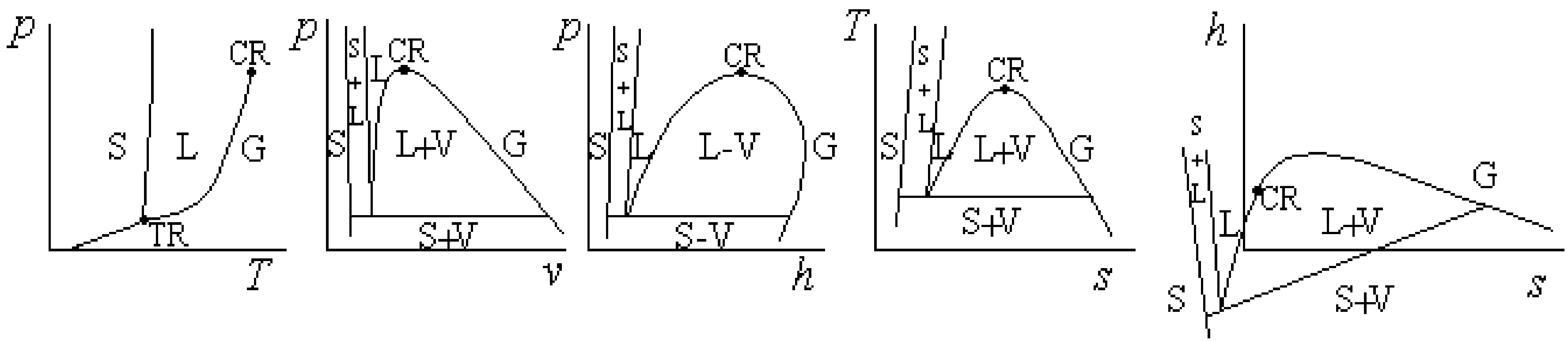
- **Thermodynamic processes in engines**





Carnot cycle Otto cycle

Phase diagrams (pure substance)



- **Normal freezing and boiling points (p_0=100 kPa)**
- **Triple point (for water T_{TR}=273.16 K, p_{TR}=611 Pa)**
- **Critical point (for water T_{CR}=647.3 K, p_{TR}=22.1 MPa)**
- **Clapeyron's equation (for water h_{SL}=334 kJ/kg, h_{LV}=2260 kJ/kg)**

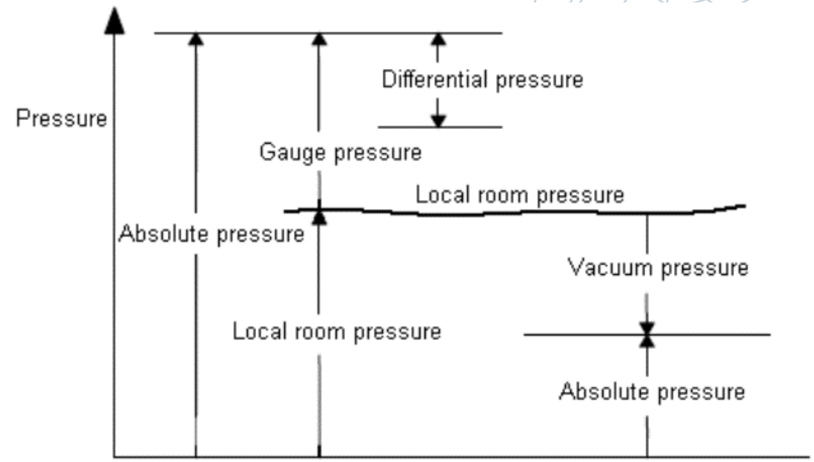
$$\left.\frac{dp}{dT}\right|_{sat} = \frac{h_V - h_L}{T(v_V - v_L)} \xrightarrow{v_V >> v_L,\, v_V = RT/p,\, h_{LV} = const} \ln\left(\frac{p}{p_0}\right) = \frac{-h_{LV}}{R}\left(\frac{1}{T} - \frac{1}{T_0}\right)$$

Thermometry

- **Temperature, the thermal level of a system, can be measured by different primary means:**
  - The ideal-gas, constant-volume thermometer $$\frac{T}{T_{TPW}} \equiv \lim_{p\to 0} \frac{pV}{(pV)_{TPW}}$$
  - The acoustic gas thermometer
  - The spectral radiation thermometer $$\frac{T}{T_{TPW}} \equiv \lim_{\varepsilon\to 1} \left(\frac{M}{M_{TPW}}\right)^{1/4}$$
  - The total radiation thermometer
  - The electronic noise thermometer
- **The temperature unit is chosen such that $T_{TPW} \equiv 273.16$ K**
- **The Celsius scale is defined by T/ºC ≡ T/K-273.15**
- **Practical thermometers:**
  - Thermoresistances (e.g. Pt100, NTC)
  - Thermocouples (K,J…).

Piezometry

- Pressure (normal surface force per unit normal area), is a scalar magnitude measured by difference (in non-isolated systems; recall free-body force diagrams).
- Gauge and absolute pressure:



- Pressure unit (SI) is the pascal, 1 Pa≡1 N/m² (1 bar≡100 kPa)
- Hydrostatic equation:

$$\frac{dp}{dz} = -\rho g \rightarrow \begin{cases} \xrightarrow{PLM} & p = p_0 - \rho g (z - z_0) \\ \xrightarrow{PGM} & \dfrac{dp}{dz} = -\dfrac{p}{RT} g \end{cases}$$

- Vacuum (practical limit is about 10^{-8} Pa)
- Pressure sensors: U-tube, Bourdon tube, diaphragm, piezoelectric…

Questions

(Only one answer is correct)

1. **The mass of air in a 30 litre vessel at 27 ºC and a gauge pressure of 187 kPa is about?**
   a) 1 g
   b) 10 g
   c) 100 g
   d) 1000 g..
2. **When a gas in a 30 litre rigid vessel is heated from 50 ºC to 100 ºC, the pressure ratio: (final/initial):**
   a) Doubles
   b) Is closer to 1 than to 2.
   c) Depends on initial volume
   d) Depends on heating speed
3. **Liquids:**
   a) Cannot be compressed
   b) Cannot be heated by compression
   c) Heat a little bit when compressed, but volume remains the same
   d) Heat up and shrink when compressed
4. **The critical temperature of any gas is:**
   a) The temperature below which the gas cannot exist as a liquid
   b) -273.16 ºC
   c) The temperature above which the gas cannot be liquefied
   d) The temperature at which solid, liquid, and gas coexist
5. **In a refrigerator, the amount of heat extracted from the cold side:**
   a) Cannot be larger than the work consumed
   b) Cannot be larger than the heat rejected to the hot side
   c) Is inversely proportional to the temperature of the cold side
   d) Is proportional to the temperature of the cold side.

Questions

(Only one answer is correct)

6. **Which of the following assertions is correct?**
   a) Heat is proportional to temperature
   b) Heat is a body's thermal energy
   c) Net heat is converted to net work in a heat engine
   d) The algebraic sum of received heats in an interaction of two bodies must be null.
7. **The variation of entropy in a gas when it is compressed in a reversible way is:**
   a) Less than zero
   b) Equal to zero
   c) Greater than zero
   d) It depends on the process.
8. **The volumetric coefficient of thermal expansion:**
   a) Is always positive
   b) Is dimensionless
   c) Is different in the Kelvin and Celsius temperature scales
   d) Is three times the linear coefficient value.
9. **It is not possible to boil an egg in the Everest because:**
   a) The air is too cold to boil water
   b) Air pressure is too low for stoves to burn
   c) Boiling water is not hot enough
   d) Water cannot be boiled at high altitudes.
10. **When a combustion takes place inside a rigid and adiabatic vessel:**
   a) Internal energy increases
   b) Internal energy variation is null
   c) Energy is not conserved
   d) Heat flows out.

Exercises

1. **A U-tube is made by joining two 1 m vertical glass-tubes of 3 mm bore (6 mm external diameter) with a short tube at the bottom. Water is poured until the liquid fills 600 mm in each column. Then, one end is closed. Find:**
    1. The change in menisci height due to an ambient pressure change, $(\partial z/\partial p_{amb})$, with application to Δp=1 kPa.
    2. The change in menisci height due to an ambient temperature change, $(\partial z/\partial T_{amb})$, with application to ΔT=5 ºC.
2. **An aluminium block of 54.5 g, heated in boiling water, is put in a calorimeter with 150 cm^3 of water at 22 ºC, with the thermometer attaining a maximum of 27.5 ºC after a while. Find the thermal capacity of aluminium.**
3. **How many ice cubes of 33 g each, at -20 ºC, are required to cool 1 litre of tea from 100 ºC to 0 ºC?**
4. **Carbon dioxide is trapped inside a vertical cylinder 25 cm in diameter by a piston that holds internal pressure at 120 kPa. The plunger is initially 0.5 m from the cylinder bottom, and the gas is at 15 ºC. Thence, an electrical heater inside is plugged to 220 V, and the volume increases by 50% after 3 minutes. Neglecting heat losses through all walls, and piston friction, find:**
    1. The energy balance for the gas and for the heater.
    2. The final temperature and work delivered or received by the gas.
5. **Find the air stagnation temperature on leading edges of an aircraft flying at 2000 km/h in air at -60 ºC.**

Master
in Space Science and Technology

Thermal engineering

Isidoro Martínez

Thermal engineering

- **Thermodynamics**
  - Basic (energy and entropy, state properties, state equations, simple processes, phase changes)
  - Applied (mixtures, liquid-vapour equilibrium, air conditioning, thermochemistry, power and cold generation, materials processes)

- **Heat transfer**
  - Thermal conduction (solids…)
  - Thermal convection (fluids…)
  - Thermal radiation (vacuum…)
  - Heat exchangers
  - Heat generation (electrical heaters…)
  - Thermal control systems
  - Combined heat and mass transfer (evaporative cooling, ablation…)

Heat transfer

- **What is heat (i.e. heat flow, heat transfer)?**
  - First law: *heat is non-work energy-transfer through an impermeable surf.*

$$Q \equiv \Delta E - W = \Delta E + \int p\mathrm{d}V - W_{dis} = \Delta H - \int V\mathrm{d}p - W_{dis} = \left(mc\Delta T\right)_{\text{PIS,non-dis}}$$

  - Second law: heat tends to equilibrate the temperature field.

$$\dot{s}_{gen} = \frac{-\nabla T \cdot \vec{\dot{q}}}{T^2}$$

- **What is heat flux (i.e. heat flow rate, heat transfer rate)?**

$$\dot{Q} \equiv \frac{dQ}{dt} = mc\left.\frac{dT}{dt}\right|_{\text{PSM,non-dis}} \equiv KA\Delta T$$

- ***<u>Heat transfer</u> is the flow of thermal energy driven by thermal non-equilibrium (i.e. the effect of a non-uniform temperature field), commonly measured as a heat flux (vector field).***

Heat transfer modes

- **How is heat flux density modelled?**

$$\dot{q} \equiv \frac{\dot{Q}}{A} = K\Delta T \begin{cases} \text{conduction} & \vec{\dot{q}} = -k\nabla T \\ \text{convection} & \dot{q} \equiv h\left(T - T_\infty\right) \\ \text{radiation} & \dot{q} = \varepsilon\sigma\left(T^4 - T_\infty^4\right) \end{cases}$$

  - The 3 ways to change $\dot{Q}$: *K*, *A*, and ΔT.
  - *K* is thermal conductance coeff. (or heat transfer coeff.), *k* is conductivity, *h* is convective coeff., ε is emissivity.
  - Field or interface variables?
  - Vector or scalar equations?
  - Linear or non-linear equations?
  - Material or configuration properties?
  - Which emissivity? This form only applies to bodies in large enclosures.

Heat conduction

- **Physical transport mechanism**
  - –Short-range atomic interactions (collision of particles in fluids, or phonon waves in solids), supplemented with free-electron flow in metals.
- **Fourier's law (1822)**

$$\vec{\dot{q}} = -k\nabla T$$

- **Heat equation**

$$\left.\frac{dH}{dt}\right|_p = \dot{Q} \rightarrow \int_V \rho c \frac{\partial T}{\partial t} dV = -\int_A \vec{\dot{q}} \cdot \vec{n} dA + \int_V \phi dV = -\int_V \nabla \cdot \vec{\dot{q}}\, dV + \int_V \phi dV$$

$$\xrightarrow{V\to 0} \rho c \frac{\partial T}{\partial t} = -\nabla \cdot \vec{\dot{q}} + \phi \overset{\nabla k=0}{=} k\nabla^2 T + \phi, \quad \text{or} \quad \frac{\partial T}{\partial t} = a\nabla^2 T + \frac{\phi}{\rho c}$$

–with the initial and boundary conditions particular to each problem.

Thermal conductivity

Table 1. Representative thermal conductivity values

	k [W/(m·K)]	Comments
Order of magnitude for solids	10^2 (good conductors) 1 (bad conductors)	In metals, Lorentz's law (1881), $k/(\sigma T)$=constant
Aluminium	200	Duralumin has k=174 W/(m·K), increasing to k=188 W/(m·K) at 500 K.
Iron and steel	50 (carbon steel) 20 (stainless steel)	Increases with temperature. Decreases with alloying
Order of magnitude for liquids	1 (inorganic) 0.1 (organic)	Poor conductors (except liquid metals).
Water	0.6	Ice has k=2.3 W/(m·K),
Order of magnitude for gases	10^{-2}	Very poor thermal conductors. KTG predicts $k/(\rho c)\equiv a=D_i=\nu\approx10^{-5}$ m^2/s
Air	0.024	Super insulators must be air evacuated.

Simple heat conduction cases

- **One-dimensional steady cases**
  - Planar $\dot{Q} = kA\frac{T_1 - T_2}{L_{12}}$
  - Cylindrical $\dot{Q} = k2\pi L\frac{T_1 - T_2}{\ln\frac{R_2}{R_1}}$
  - Spherical $\dot{Q} = k4\pi R_1 R_2\frac{T_1 - T_2}{R_2 - R_1}$

- **Composite wall (planar multilayer)**

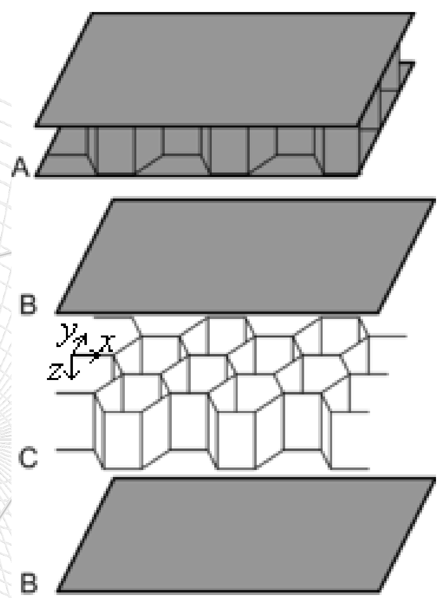
$$\dot{q} = K\Delta T = k_{12}\frac{T_2 - T_1}{L_{12}} = k_{23}\frac{T_3 - T_2}{L_{23}} = \ldots = \frac{T_n - T_1}{\sum\frac{L_i}{k_i}} \quad \Rightarrow \quad K = \frac{1}{\sum\frac{L_i}{k_i}}$$

- **Unsteady case. Relaxation time:**

$$\Delta t = mc\Delta T / \dot{Q} \quad \begin{cases} \Delta t \overset{Bi>>1}{=} \frac{\rho c L^2}{k} \\ \Delta t \overset{Bi<<1}{=} \frac{\rho c V}{hA} \end{cases} \quad Bi \equiv \frac{hL}{k_S}$$

Multiple path in heat conduction

- **Multidimensional analysis**
  - Analytical, e.g. separation of variables, conduction shape factors,
  - Numerical, finite differences, lumped network, finite elements
- **Parallel thermal resistances**
  - Example: honeycomb panel made of ribbon (thickness δ), cell size s:



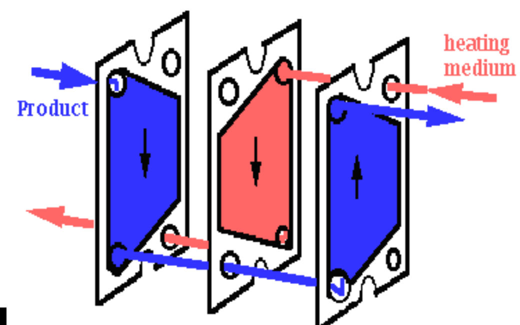
$$\left.\begin{aligned}
\dot{Q}_x &= kF_x A_x \frac{\Delta T_x}{L_x} \quad \text{with} \quad F_x = \frac{3}{2}\frac{\delta}{s} \\
\dot{Q}_y &= kF_y A_y \frac{\Delta T_y}{L_y} \quad \text{with} \quad F_y = \frac{\delta}{s} \\
\dot{Q}_z &= kF_z A_z \frac{\Delta T_z}{L_z} \quad \text{with} \quad F_z = \frac{8}{3}\frac{\delta}{s}
\end{aligned}\right\}$$

Heat convection

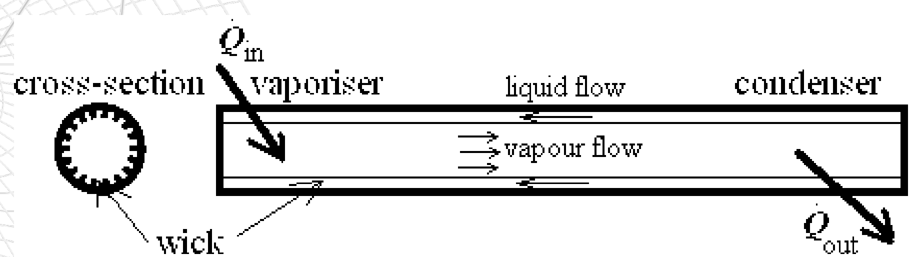
- **Newton's law and physical mechanism**

$$\dot{q} \equiv h\left(T-T_{\infty}\right)=-k\nabla_{n}T \quad \rightarrow \quad h\Delta T \approx k\frac{\Delta T}{\delta} \quad \rightarrow \quad Nu \equiv \frac{hL}{k}=f\left(Re,Pr...\right)$$

  - e.g. in air flow, $h=a+bv_{wind}$, with a=3 W/(m²·K) and b=3 J/(m³·K)
  - e.g. plate (<1 m)at rest, $h=a(T-T_{\infty})^{1/4}$, with $a\sim2$ W/(m²·K⁵/⁴) (1,6 upper, 0.8 lower, 1.8 vert.)
- **Classification of heat convection problems**
  - By time change: steady, unsteady (e.g. onset of convection)
  - By flow origin: forced (flow), natural (thermal, solutal…)
  - By flow regime: laminar, turbulent
  - By flow topology: internal flow, external flow
  - By flow phase: single-phase or multi-phase flow
- **Heat exchangers (tube-and-shell, plates…)**



- **Heat pipes**



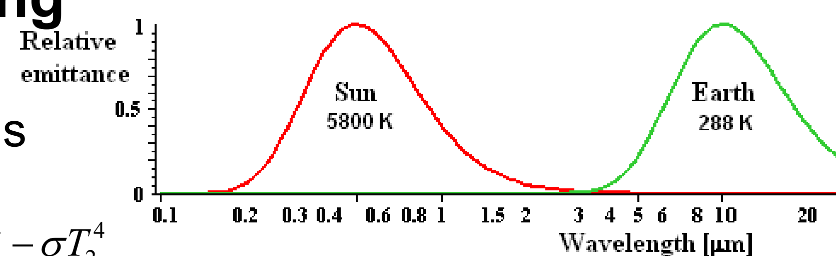
Heat radiation

- **Heat radiation (thermal radiation)**
  - It is the transfer of internal thermal energy to electromagnetic field energy, or viceversa, modelled from the basic black-body theory. Electromagnetic radiation is emitted as a result of the motion of electric charges in atoms and molecules.
- **Blackbody radiation**
  - Radiation within a vacuum cavity
    - Radiation temperature (equilibrium with matter)
    - Photon gas (wave-particle duality, carriers with zero rest mass, $E=h\nu$, $p=E/c$)
    - Isotropic, unpolarised, incoherent spatial distribution
    - Spectral distribution of photon energies at equilibrium (E=const., S=max.)
  - Radiation escaping from a hole in a cavity
    - Blackbody emmision

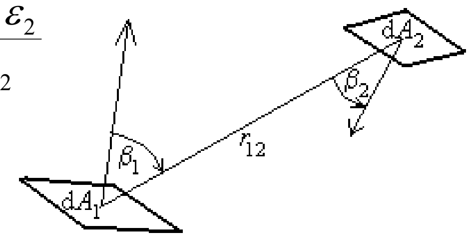
$$M_\lambda = \frac{2\pi h c^2}{\lambda^5\left[\exp\left(\frac{hc}{k\lambda T}\right)-1\right]} \quad \begin{cases} M = \int_0^\infty M_\lambda \mathrm{d}\lambda = \sigma T^4 & \sigma = 5.67\cdot 10^{-8}\ \dfrac{\mathrm{W}}{\mathrm{m}^2\cdot\mathrm{K}^4} \\ \lambda\big|_{M_\lambda=\max} = \dfrac{C}{T} & C = 0.003\ \mathrm{m}\cdot\mathrm{K} \end{cases}$$

Thermo-optical properties

- **Propagation through real media**
  - Attenuation by absorption and scattering (Rayleigh if $d<<\lambda$, Mie if $d\geq\lambda$)
- **Properties of real surfaces**
  - Partial absorption (α), reflectance (ρ), emissivity (ε), and, in some cases, transmittance (τ). Energy balance: $\alpha+\rho+\tau=1$.
  - Directional and spectral effects (e.g. retroreflective surfaces, selective glasses…)
  - Detailed equilibrium: Kirchhoff's law (1859), $\alpha_{\lambda\beta\theta T}=\varepsilon_{\lambda\beta\theta T}$, but usually $\alpha\neq\varepsilon$
- **Spectral and directional modelling**
  - Two-spectral-band model:
  - Diffuse (cosine law) or specular models



- **Radiative coupling**
  - e.g. planar infinite surfaces: $\dot{q}_{12}=\dfrac{\sigma T_1^4-\sigma T_2^4}{\dfrac{1-\varepsilon_1}{\varepsilon_1}+1+\dfrac{1-\varepsilon_2}{\varepsilon_2}}$
- **View factors** $F_{12}=\dfrac{1}{\pi A_1}\displaystyle\int_{A_2}\int_{A_1}\dfrac{\cos\beta_1\cos\beta_2}{r_{12}^2}dA_1dA_2$



Heat transfer goals

- **Analysis**
  - –Find the heat flux for a given set-up and *temperature* field
    e.g. $\dot{Q} = kA\left(T_1 - T_2\right)/L$
  - –Find the temperature corresponding to a given heat flux and set-up
    e.g. $T_1 = T_2 + \dot{Q}L/\left(kA\right)$
- **Design**
  - –Find an appropriate material that allows a prescribed heat flux with a given *T*-field in a given geometry
    e.g. $k = \dot{Q}L/\left(A\Delta T\right)$
  - –Find the thickness of insulation to achieve a certain heat flux with a given *T*-field in a prescribed geometry
    e.g. $L = kA\left(T_1 - T_2\right)/\dot{Q}$
- **Control**
  - -To prevent high temperatures, use insulation and radiation shields, or use heat sinks and coolers.
  - –To prevent low temperatures, use insulation and radiation shields, or use heaters.
  - –To soften transients, increase thermal inertia (higher thermal capacity, phase change materials).

Application to electronics cooling

- All active electrical devices at steady state must evacuate the energy dissipated by Joule effect (i.e. need of heat sinks).
- Most electronics failures are due to overheating (e.g. for germanium at T>100 ºC, for silicon at T>125 ºC).
- At any working temperature there is always some dopant diffusion at junctions and bond-material creeping, causing random electrical failures, with an event-rate doubling every 10 ºC of temperature increase. Need of thermal control.
- Computing power is limited by the difficulty to evacuate the energy dissipation (a Pentium 4 CPU at 2 GHz in 0.18 μm technology must dissipate 76 W in an environment at 40 ºC without surpassing 75 ºC at the case, 125 ºC at junctions).
- Modern electronic equipment, being powerfull and of small size, usually require liquid cooling (e.g. heat pipes).

Thermal modelling

- **Modelling the geometry**
- **Modelling the material properties**
- **Modelling the transients**
- **Modelling the heat equation**
- **Mathematical solution of the model**
  - Analytical solutions
  - Numerical solutions
- **Analysis of the results**
- **Verification planning (analytical checks and testing)**
- **Feedback**

Questions

(Only one answer is correct)

1. **The steady temperature profile in heat transfer along a compound wall:**
   a) Has discontinuities
   b) Must have inflexion points
   c) Must be monotonously increasing or decreasing
   d) Must have a continuous derivative.
2. **If the temperature at the hot side of a wall is doubled:**
   a) Heat flow through the wall doubles
   b) Heat flow through the wall increases by a factor of 4
   c) Heat flow through the wall increases by a factor of 8
   d) None of the above.
3. **When a piece of material is exposed to the sun, its temperature rises until:**
   a) It loses and gains heat at the same rate
   b) The heat absorbed equals its thermal capacity
   c) It reflects all the energy that strikes it
   d) No more heat is absorbed.
4. **A certain blackbody at 100 ºC radiates 100 W. How much radiates at 200 ºC?**
   a) 200 W
   b) 400 W
   c) 800 W
   d) None of the above.
5. **When two spheres, with same properties except for their radius, are exposed to the Sun and empty space:**
   a) The larger one gets hotter
   b) The larger one gets colder
   c) The larger one gets hotter or cooler depending on their emissivity-to-absorptance ratio
   d) None of the above.

Exercises

1. **A small frustrum cone 5 cm long, made of copper, connects two metallic plates, one at 300 K in contact with the smallest face, which is 1 cm in diameter, and the other at 400 K, at the other face, which is 3 cm in diameter. Assuming steady state, quasi-one-dimensional flow, and no lateral losses, find:**
   - The temperature profile along the axis.
   - The heat flow rate.
2. **An electronics board 100·150·1 mm^3 in size, made of glass fibre laminated with epoxy, and having *k*=0.25 W/(m·K), must dissipate 5 W from its components, which are assumed uniformly distributed. The board is connected at the largest edges to high conducting supports held at 30 ºC. Find:**
   1. The maximum temperature along the board, if only heat conduction at the edges is accounted for (no convection or radiation losses).
   2. The thickness of a one-side copper layer (bonded to the glass-fibre board) required for the maximum temperature to be below 40 ºC above that of the supports.
   3. The transient temperature field, with and without a convective coefficient of h=2 W/(m^2·K).
3. **Find the required area for a vertical plate at 65 ºC to communicate 1 kW to ambient air at 15 ºC.**
4. **Consider two infinite parallel plates, one at 1000 ºC with ε=0.8 and the other at 100 ºC with ε=0.7. Find:**
   - The heat flux exchanged.
   - The effect of interposing a thin blackbody plate in between.
5. **Find the steady temperature at 1 AU, for an isothermal blackbody exposed to solar and microwave background radiation, for the following geometries: planar one-side surface (i.e. rear insulated), plate, cylinder, sphere, and cube.**

(END)

Referencias

- http://imartinez.etsiae.upm.es/~isidoro//
- Martínez, I., "Termodinámica básica y aplicada", Dossat, 1992.
- Wark, K., "Thermodynamics", McGraw-Hill, 1999. Versión española Edit. McGraw-Hill, 2000.
- Holman, J.P., "Heat transfer", McGraw-Hill, 2010.
- Gilmore, D.G., “Satellite Thermal Control Handbook”, The Aerospace Corporation Press, 1994.
- www.electronics-cooling.com