

(Function values at 100 kPa and 288 K or the normal boiling temperature if greater.)

Substance	Formula	Molar mass	Boiling temp.	Critical temp	Critical pressure	Critical compressibility factor <sup>a</sup>	Pitzer's acentric factor	Thermal capacity <sup>b</sup>	Thermal conductivity <sup>c</sup>	Dynamic viscosity <sup>d</sup>
		M kg/mol	$T_b$ K	$T_{cr}$ K	$p_{cr}$ MPa	$Z_{cr}$	$\omega$	$c_p$ J/(kg·K)	$k$ W/(m·K)	$\mu \cdot 10^6$ Pa·s
Acetone	C <sub>3</sub> H <sub>6</sub> O	0.058	329.2	508	4.70	0.233	0.309	1300		
Acetylene	C <sub>2</sub> H <sub>2</sub>	0.026	189.5 <sup>f</sup>	309	6.20	0.271	0.184	1580	0.019	9.3
Air	79%N <sub>2</sub> + 21%O <sub>2</sub>	0.029	82 <sup>e</sup>	132 <sup>g</sup>	3.75 <sup>g</sup>	0.28 <sup>g</sup>	0.035	1004	0.024	18.1
Ammonia	NH <sub>3</sub>	0.017	239.8	406	11.30	0.242	0.250	2200	0.022	9.3
Argon	Ar	0.040	87.4	151	4.86	0.291	0	523	0.018	21.0
Benzene	C <sub>6</sub> H <sub>6</sub>	0.078	353.3	563	4.92	0.271	0.212	1300	0.007	7.0
1,3-Butadiene	C <sub>4</sub> H <sub>6</sub>	0.054	268.5	425	4.33	0.270	0.193	1510		
n-Butane	C <sub>4</sub> H <sub>10</sub>	0.058	272.6	425	3.80	0.274	0.193	1580	0.015	7.0
iso-Butane	C <sub>4</sub> H <sub>10</sub>	0.058	261.5	408	3.64	0.280	0.176	1580	0.015	9.0
Carbon dioxide	CO <sub>2</sub>	0.044	194.7 <sup>f</sup>	304	7.38	0.274	0.225	840 <sup>h</sup>	0.016	14.4
Carbon monoxide	CO	0.028	81.7	133	3.50	0.295	0.049	1100	0.023	17.0
Carbon tetrachloride	CCl <sub>4</sub>	0.154	349.7	556	4.56	0.272	0.194	862	0.017	16.0
Cyclohexane	C <sub>6</sub> H <sub>12</sub>	0.084	353.9	554	4.07	0.273	0.212			
n-Decane	C <sub>10</sub> H <sub>22</sub>	0.142	447.3	619	2.12	0.247	0.490	1680		
n-Dodecane	C <sub>12</sub> H <sub>26</sub>	0.170	489.4	659	1.80	0.240	0.562	1690		
DME (dimethyl ether)	C <sub>2</sub> H <sub>6</sub> O	0.046	250.6	400	5.37	0.271	0.274	1430		
Ethane	C <sub>2</sub> H <sub>6</sub>	0.030	184.6	305	4.88	0.285	0.100	1700	0.020	11.0
Ethanol	C <sub>2</sub> H <sub>6</sub> O	0.046	351.5	516	6.39	0.248	0.635	1520	0.013	14.2
Ether (diethyl ether)	C <sub>4</sub> H <sub>10</sub> O	0.074	307.6	467	3.61	0.260	0.281	1600	0.015	7.5
ETBE (ethyl tert-butyl ether)	C <sub>6</sub> H <sub>14</sub> O	0.102	345	517	3.11	0.274	0.298	1550		
Ethylene	C <sub>2</sub> H <sub>4</sub>	0.028	169.5	283	5.12	0.276	0.085	1470	0.018	9.6
Ethylene glycol	C <sub>2</sub> H <sub>6</sub> O <sub>2</sub>	0.062	471	645	7.53	0.268	1.137	1410		
Helium ( <sup>4</sup> He)	He	0.004	4.2	5.3	0.23	0.301	-0.387	5190	0.142	19.0
Helium 3 ( <sup>3</sup> He)	He	0.003	3.2	3.3	0.11	0.301	-0.460			
n-Heptane	C <sub>7</sub> H <sub>16</sub>	0.100	371	540	2.77	0.263	0.350	1650	0.013	6.5
n-Hexane	C <sub>6</sub> H <sub>14</sub>	0.086	342	508	3.03	0.263	0.296	1700	0.014	6.5
Hydrazine	N <sub>2</sub> H <sub>4</sub>	0.032	387	653	14.7	0.376	0.325			
Hydrogen	H <sub>2</sub>	0.002	20.1	33	1.32	0.305	-0.22	14200	0.168	8.4
(Hydrogen) Deuterium	D <sub>2</sub>	0.004	23.6	38	1.66	0.249	-0.16	14200	0.131	12
Hydrogen peroxide <sup>i</sup>	H <sub>2</sub> O <sub>2</sub>	0.034	272.7	728 <sup>i</sup>	22			1270		
Mercury <sup>j</sup>	Hg	0.201	630	736	104					
Methane	CH <sub>4</sub>	0.016	112	191	4.60	0.288	0.010	2180	0.031	10.3
Methanol	CH <sub>4</sub> O	0.032	338.1	513	8.08	0.224	0.559	1350	0.015	9.8
MTBE (methyl tert-butyl ether)	C <sub>5</sub> H <sub>12</sub> O	0.088	328	497	3.43	0.273	0.267	1500		

Neon	Ne	0.020	26.2	44	2.70	0.301	0	1030	0.046	30.0
Nitrogen	N <sub>2</sub>	0.028	77.4	126	3.39	0.290	0.038	1040	0.024	16.6
Nitrogen dioxide <sup>k</sup>	NO <sub>2</sub>	0.046	294.4	431	10.1	0.233		800	0.017	130
Nitrogen monoxide	NO	0.030	121.2	180	6.55	0.250	0.607	996	0.024	29.4
di-Nitrogen oxide <sup>l</sup>	N <sub>2</sub> O	0.044	184.7	310	7.25	0.272	0.160	864	0.015	13.6
n-Octane	C <sub>8</sub> H <sub>18</sub>	0.114	399	569	2.49	0.259	0.394	1700	0.020	7.5
iso-Octane	C <sub>8</sub> H <sub>18</sub>	0.114	372	544	2.59	0.267		1650		
Ozone	O <sub>3</sub>	0.048	161.4	268	6.78	0.272				
Oxygen	O <sub>2</sub>	0.032	90.2	155	5.08	0.288	0.021	913	0.024	19.1
iso-Pentane	C <sub>5</sub> H <sub>12</sub>	0.072	301.3	461	3.33	0.268	0.227	1680	0.015	11.7
n-Pentane	C <sub>5</sub> H <sub>12</sub>	0.072	309.2	470	3.38	0.262	0.251	1680	0.015	11.7
Phenol	C <sub>6</sub> H <sub>6</sub> O	0.094	455	694	6.13	0.243	0.426			
Propane	C <sub>3</sub> H <sub>8</sub>	0.044	231.1	370	4.26	0.281	0.152	1570	0.015	7.4
iso-Propanol	C <sub>3</sub> H <sub>8</sub> O	0.060	355.4	508	4.76	0.248	0.669	1540		
Propylene (propene)	C <sub>3</sub> H <sub>6</sub>	0.042	225.4	365	4.62	0.275	0.148	1460	0.014	8.1
Propylene glycol	C <sub>3</sub> H <sub>8</sub> O <sub>2</sub>	0.076	461.3	626	6.10	0.280	1.107			
R12 (CFC-12) (dichlorodifluoromethane)	CCl <sub>2</sub> F <sub>2</sub>	0.121	243.0	385	4.14	0.280	0.179	573	0.008	12.5
R134a (HFC-134a) (tetrafluoroethane)	CF <sub>3</sub> CH <sub>2</sub> F	0.102	246.6	374	4.07	0.258	0.330	840	0.014	12.2
R410A <sup>m</sup>	n.a.	0.073	221.8	345	4.90	0.271	0.296	820		
Sulfur dioxide	SO <sub>2</sub>	0.064	263.2	430	7.87	0.264	0.251	607	0.009	11.6
Sulfur hexafluoride <sup>n</sup>	SF <sub>6</sub>	0.146	204.9 <sup>f</sup>	319	3.76	0.360	0.210	598	0.12	16.0
Toluene	C <sub>7</sub> H <sub>8</sub>	0.092	383.7	592	4.13	0.284	0.266			
Tetradecafluorohexane	C <sub>6</sub> F <sub>14</sub>	0.338	329	449	1.83					
Uranium hexafluoride <sup>o</sup>	UF <sub>6</sub>	0.352	329 <sup>f</sup>	503	4.60	0.282	0.092	370	0.009	20
Water (steam) <sup>p</sup>	H <sub>2</sub> O	0.018	372.8	647.3	22.12	0.229	0.344	2050 <sup>p</sup>	0.025	12.1
Xenon	Xe	0.131	165.0	289.8	5.84	0.291	0	158	0.006	22.5

<sup>a</sup>Critical molar volumes can be obtained from  $v_{cr}=Z_{cr}RT_{cr}/p_{cr}$ , and critical densities from  $\rho_{cr}=M/v_{cr}$  (e.g. for acetone  $v_{cr}=209 \cdot 10^{-6} \text{ m}^3/\text{mol}$  and  $\rho_{cr}=351 \text{ kg/m}^3$ ).

<sup>b</sup>[Thermal capacities of monoatomic gases do not change with temperature, but for polyatomic gases it increases more the more atoms has the molecule.](#)

<sup>c</sup> Thermal conductivity of gases increases with the square root of temperature, decreases with the square root of molar mass, and do not change with pressure. Thermal diffusivity  $a=k/(\rho c_p)$ . According to simple generalised transport theory in gases, thermal diffusivity, mass diffusivity and kinematic viscosity of gases have the same values.

<sup>d</sup> Dynamic viscosity of gases increases with the square root of temperature, and do not change with pressure. Kinematic viscosity  $\nu=\mu/\rho$ .

<sup>e</sup> Bubble point.

<sup>f</sup> Sublimation point.

<sup>g</sup> Pseudo-critical point (Kay's model).

<sup>h</sup> Most gas properties vary a lot near the critical point, what may be here the case; e.g., for CO<sub>2</sub> gas at 288 K and 100 kPa, thermal capacity at constant pressure is  $c_p=840 \text{ J}/(\text{kg}\cdot\text{K})$ , growing at constant  $T=288 \text{ K}$  from  $c_p=833 \text{ J}/(\text{kg}\cdot\text{K})$  at very low pressure, to  $c_p=3010 \text{ J}/(\text{kg}\cdot\text{K})$  at the saturation pressure (5063 kPa). Thermal capacity in the ideal gas limit ( $p \rightarrow 0$ ) varies almost linearly (e.g.  $c_p=753 \text{ J}/(\text{kg}\cdot\text{K})$  at the triple-point temperature,  $c_p=850 \text{ J}/(\text{kg}\cdot\text{K})$  at the critical-point temperature).

<sup>i</sup> Data for [H<sub>2</sub>O<sub>2</sub>](#) pure (H<sub>2</sub>O<sub>2</sub> is most used in aqueous solutions). Critical temperature extrapolated from corresponding states theory, because H<sub>2</sub>O<sub>2</sub> decomposes violently at such high temperatures).

<sup>j</sup> Mercury is obtained by oxidation of cinnabar at some 600 °C and vapour condensation. Mercury vapour should not exceed 0.1 mg/m<sup>3</sup> in breathing air (notice that saturated air at 20 °C already contains more than that limit).

<sup>k</sup> Nitrogen dioxide, NO<sub>2</sub>, is a very toxic brown gas at normal conditions (but readily condensable,  $T_b=21.3 \text{ °C}$ ). All nitrogen oxides slowly decomposing to nitrogen and oxygen, making it difficult to keep them in pure state; besides, NO<sub>2</sub> is paramagnetic, but readily dimerises to dinitrogen tetroxide, N<sub>2</sub>O<sub>4</sub>, a diamagnetic pale-

yellow or colourless gas with double density than  $\text{NO}_2$  (e.g. when heating from above an ampoule containing  $\text{NO}_2$ , some  $\text{N}_2\text{O}_4$  is formed at the top ( $2\text{NO}_2(\text{g})=\text{N}_2\text{O}_4(\text{g})+57 \text{ kJ/mol}$ ), which can be seen sinking to the bottom because of buoyancy). The  $\text{NO}_2/\text{N}_2\text{O}_4$  equilibrium depends on temperature,  $\text{NO}_2$  being favoured at high temperatures and  $\text{N}_2\text{O}_4$  at low temperatures; when condensing (at  $21.3 \text{ }^\circ\text{C}$  at  $100 \text{ kPa}$ ), most of the liquid is  $\text{N}_2\text{O}_4$  which is colourless or pale brownish, and if solidified (at  $-11.2 \text{ }^\circ\text{C}$ ) a white solid appears. The liquid  $\text{N}_2\text{O}_4$  is a hypergolic propellant that spontaneously reacts upon contact with various forms of hydrazine, which makes the pair a popular bipropellant for spacecraft rockets.

- <sup>l</sup> Di-nitrogen oxide,  $\text{N}_2\text{O}$ , also known as nitrous oxide (NO is nitric oxide), or nitrogen hemi-oxide, or nitrogen protoxide, or laughing gas, is used in respiratory anaesthesia since the pioneering trials of Sir Humphrey Davy in 1789 shortly after its discovery by J. Priestley in 1772, as a non-flammable non-ozone-depleting propellant in aerosol cans, and as a fuel additive to enhance combustion (it liberates oxygen; if added as compressed liquid in the intake manifold, it greatly increases fuel load). It has a global warming potential (GWP) of 300 times that of  $\text{CO}_2$ , being the third contributor to anthropogenic GWP, after  $\text{CO}_2$  and  $\text{CH}_4$ .
- <sup>m</sup> R410A is a near-azeotropic mixture of R32 (difluoromethane,  $\text{CH}_2\text{F}_2$ ) and R125 (pentafluoroethane,  $\text{CHF}_2\text{CF}_3$ ), 50/50 by weight (70/30 molar), which can be approximated as a pure substance. The critical point of a binary mixture is defined as the point where  $\partial^2 g/\partial x^2$  and  $\partial^3 g/\partial x^3$  are simultaneously zero, where  $g$  is the Gibbs energy and  $x$  is the mole fraction of a component.
- <sup>n</sup> Sulfur hexafluoride is a synthetic gas used as insulator for electrical equipment (breakdown potential three times larger than air, and as a fluorine source for edging in the electronics industry. It is a non-flammable, non-toxic gas, which decomposes at  $750 \text{ K}$ ; it has low water solubility, and a very large IR absorbance (it is the most potent greenhouse gas,  $\text{GWP}=22\ 000$ ), what has been used as a trace gas for gas-leakage detection.
- <sup>o</sup> Uranium hexafluoride, perhaps the heaviest simple molecule, is the only uranium compound presently used in industrially enrichment of U-235, both on gas diffusion and on gas centrifugation processes. At room conditions, it is a white crystalline solid with a high vapour pressure ( $p_v=11 \text{ kPa}$  at  $20 \text{ }^\circ\text{C}$ ).
- <sup>p</sup> The boiling point of water at  $100 \text{ kPa}$  is  $T_b=372.75\pm 0.02 \text{ K}$  ( $99.60\pm 0.02 \text{ }^\circ\text{C}$ ), whereas at  $101.325 \text{ kPa}$  ( $1 \text{ atm}$ ) it is  $373.12\pm 0.02 \text{ K}$  ( $99.97\pm 0.02 \text{ }^\circ\text{C}$ ). Steam thermal capacity varies appreciably with  $T$  and  $p$ : at  $p\rightarrow 0$ ,  $c_p(T)$  grows almost linearly from  $1890 \text{ J/(kg}\cdot\text{K)}$  at  $100 \text{ }^\circ\text{C}$  to  $2130 \text{ J/(kg}\cdot\text{K)}$  at  $500 \text{ }^\circ\text{C}$ , but at high- $p$  it has a minimum (e.g. at  $200 \text{ kPa}$ ,  $c_p=2180 \text{ J/(kg}\cdot\text{K)}$  as saturated vapour at  $120 \text{ }^\circ\text{C}$ , drops to a minimum  $c_p=2010 \text{ J/(kg}\cdot\text{K)}$  at  $230 \text{ }^\circ\text{C}$ , and grows to match  $c_p(T,p\rightarrow 0)$  at high- $T$ , say  $c_p=2130 \text{ J/(kg}\cdot\text{K)}$  at  $500 \text{ }^\circ\text{C}$ ). For the perfect gas model in adiabatic expansion of steam, a value of  $\gamma=c_p/c_v=1.33$  is recommended.